



Value added fossil fuels: Coal To Liquids with CCS

IEA Committee on Energy Research and Technology
Sydney – Feb 2012

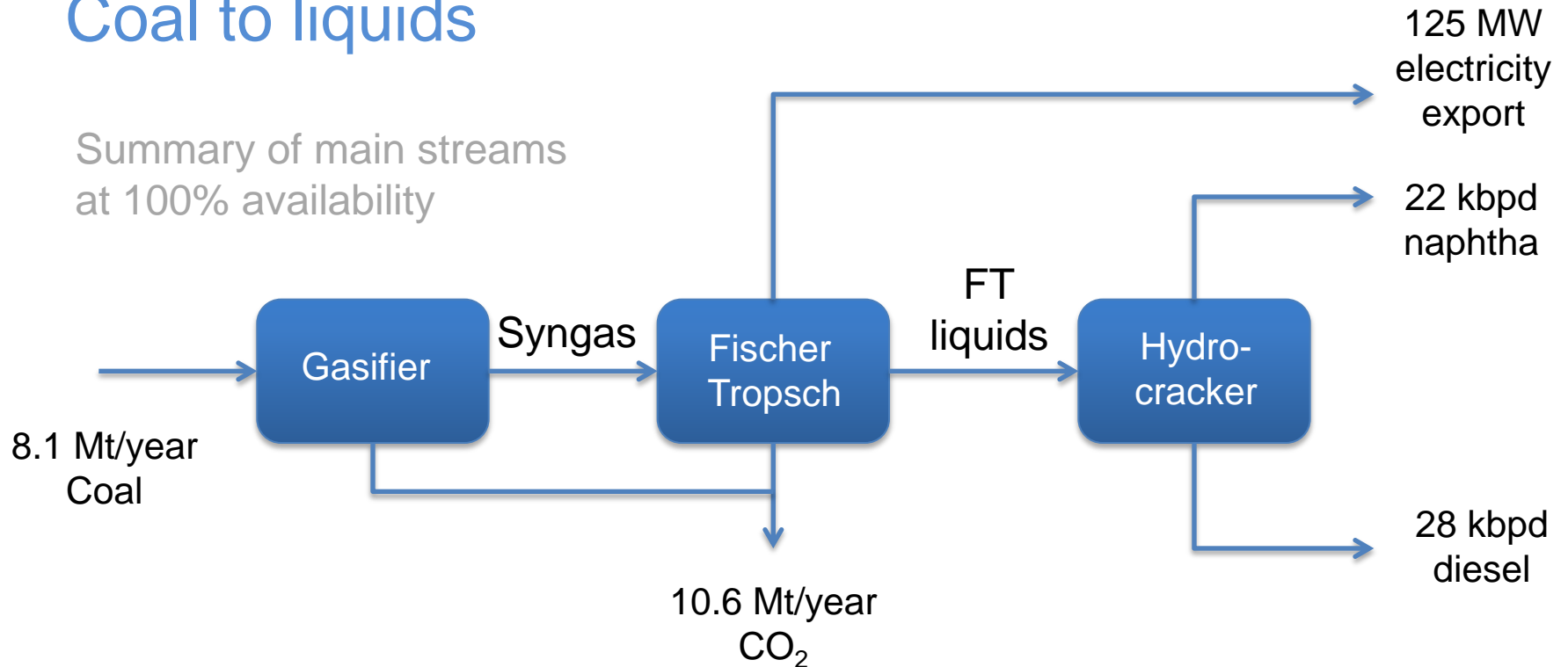
(Selected) Large scale CCS to date

Name	Type	CO2 capacity	Sink
Sleipner	Nat Gas	1 Mt/year	Saline formation
In Salah	Nat Gas	1 Mt/year	Gas reservoir
Weyburn/Midale	Substitute NG	2.5 Mt/year	EOR - pipeline
Snøhvit	Nat Gas	0.7 Mt/year	Saline formation
<i>Gorgon</i>	<i>Nat Gas</i>	<i>>3 Mt/year</i>	<i>Saline formation</i>
<i>Mississippi Power</i>	IGCC	<i>3 Mt/year</i>	<i>EOR – pipeline</i>
<i>Medicine Bow Power and Fuels</i>	<i>CTL</i>	<i>4 Mt/year</i>	<i>EOR - pipeline</i>

Italics – not yet in operation

Coal to liquids

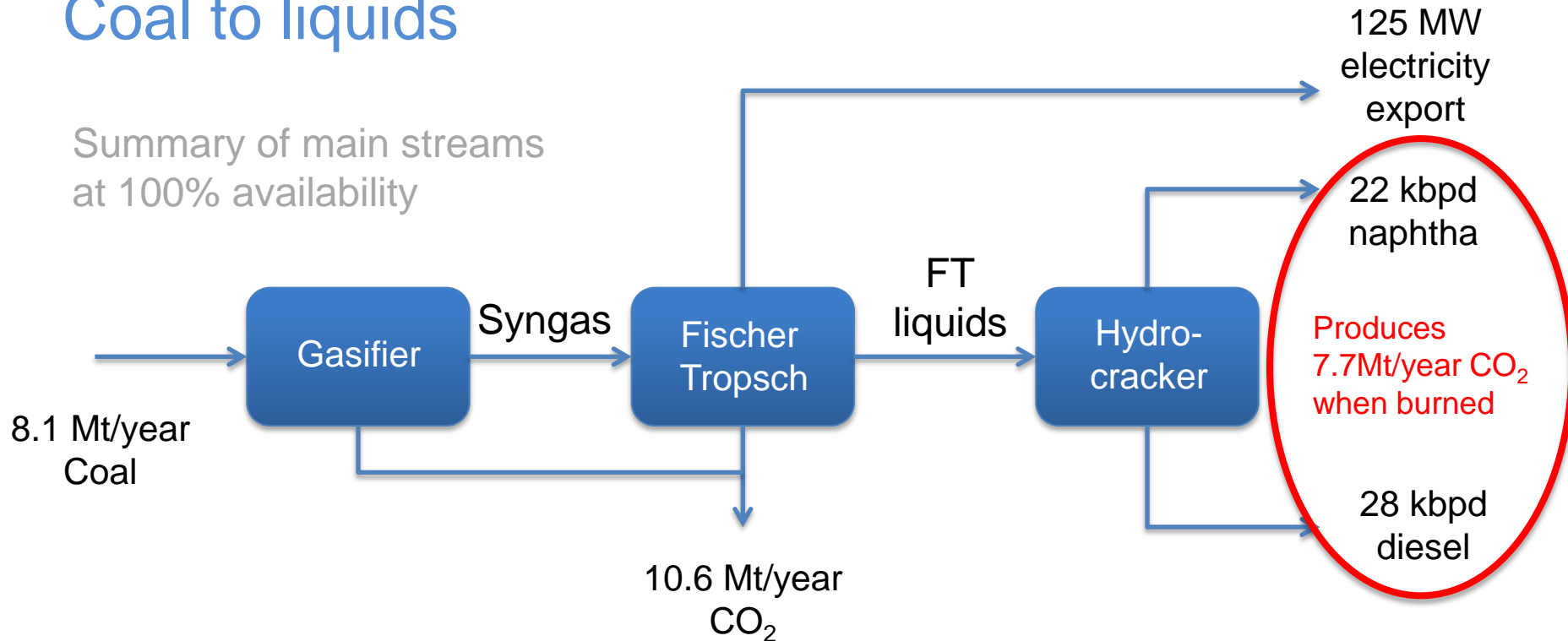
Summary of main streams at 100% availability



Source: Baseline technical and Economic Assessment of a Commercial Scale Fischer-Tropsch Liquids Facility DOE/NETL-2007/1260

Coal to liquids

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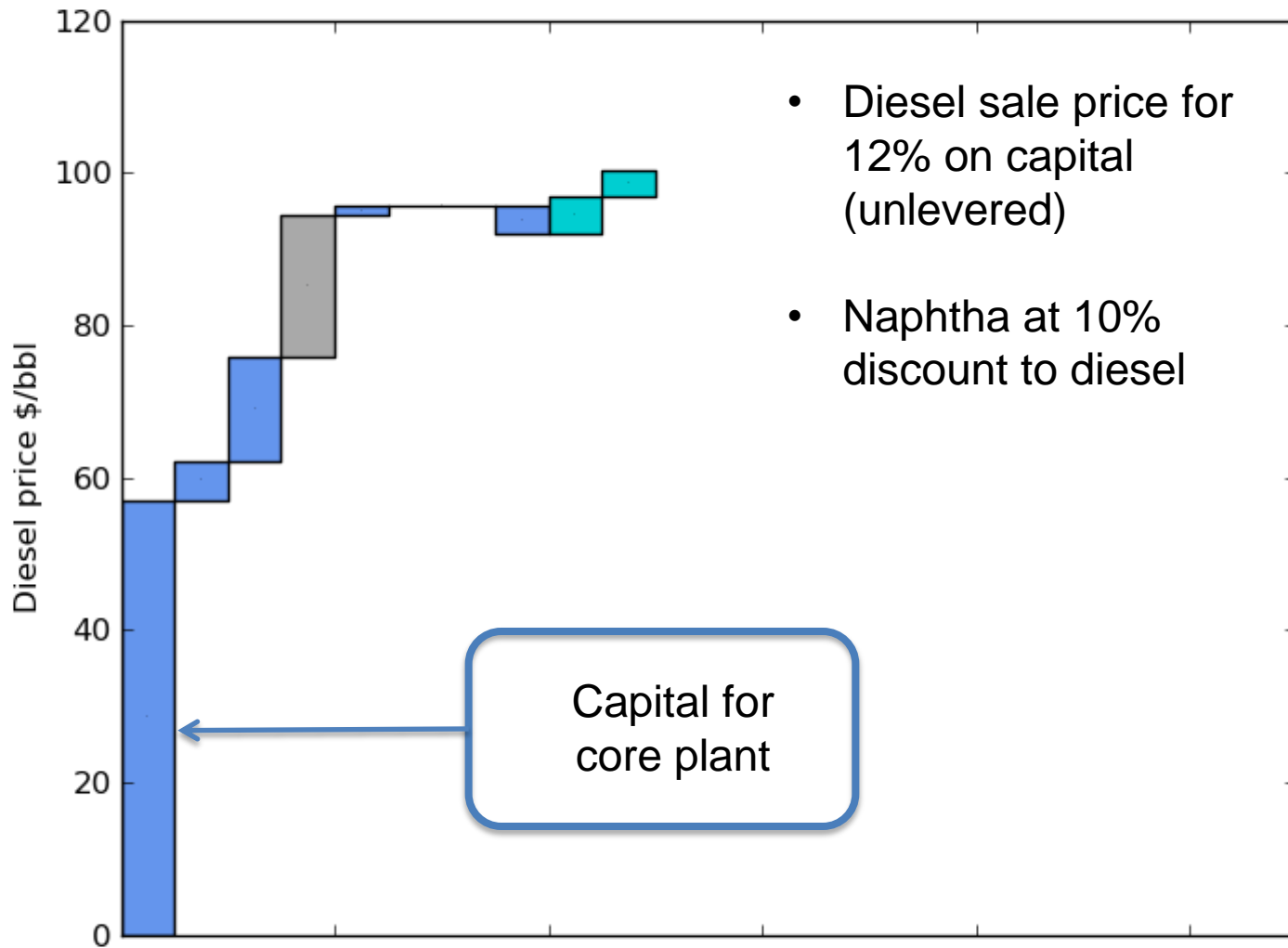
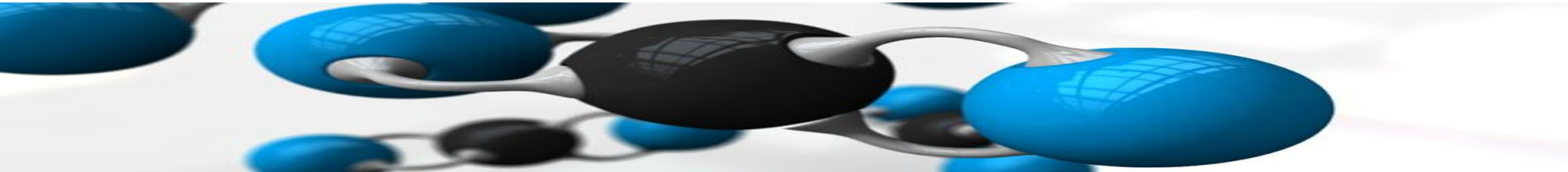


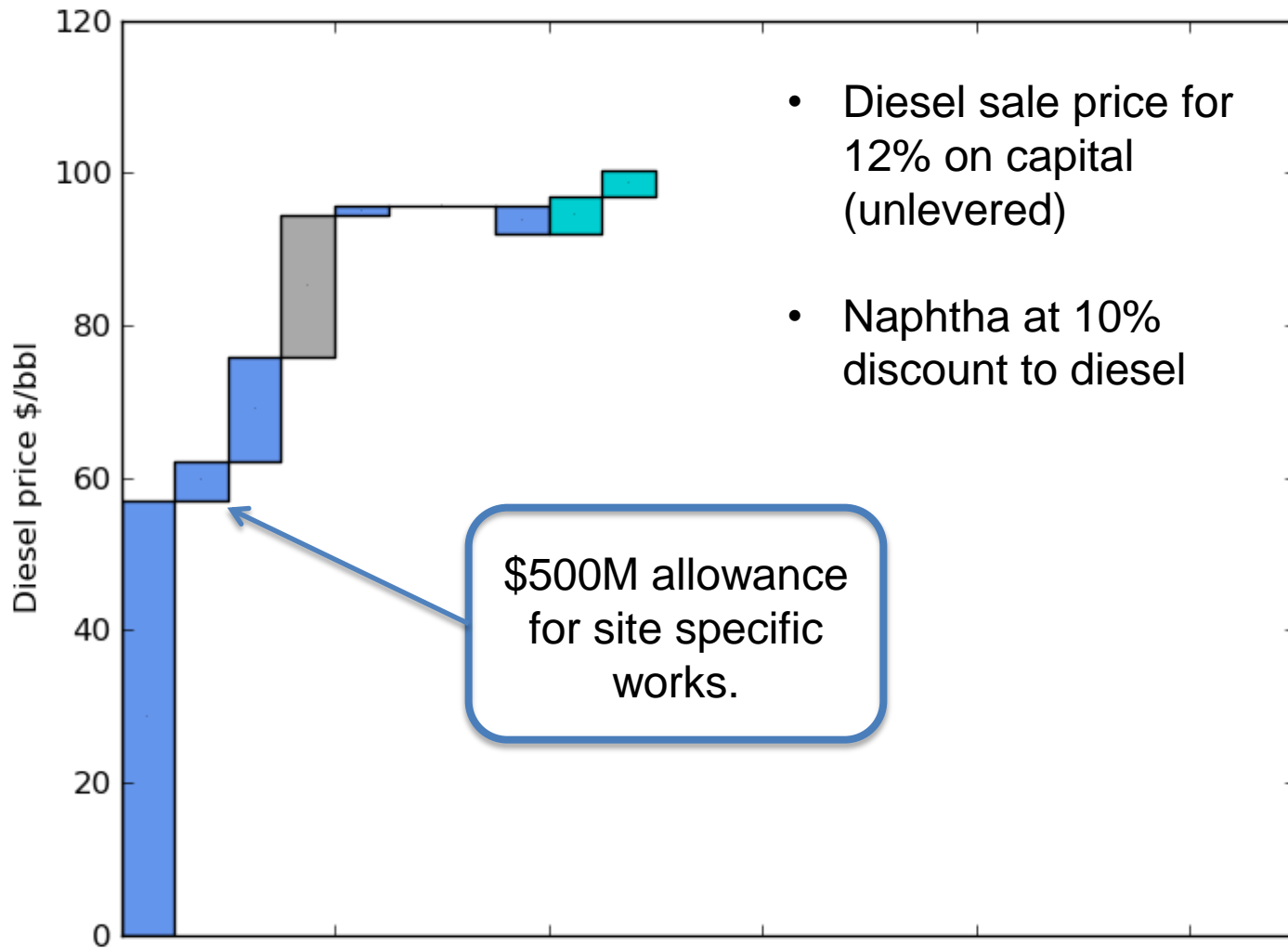
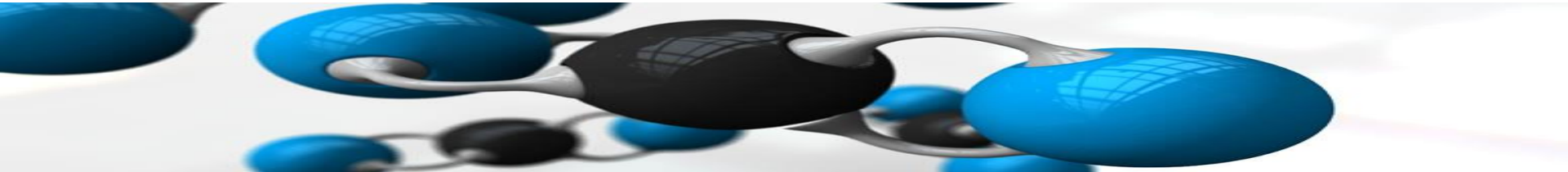
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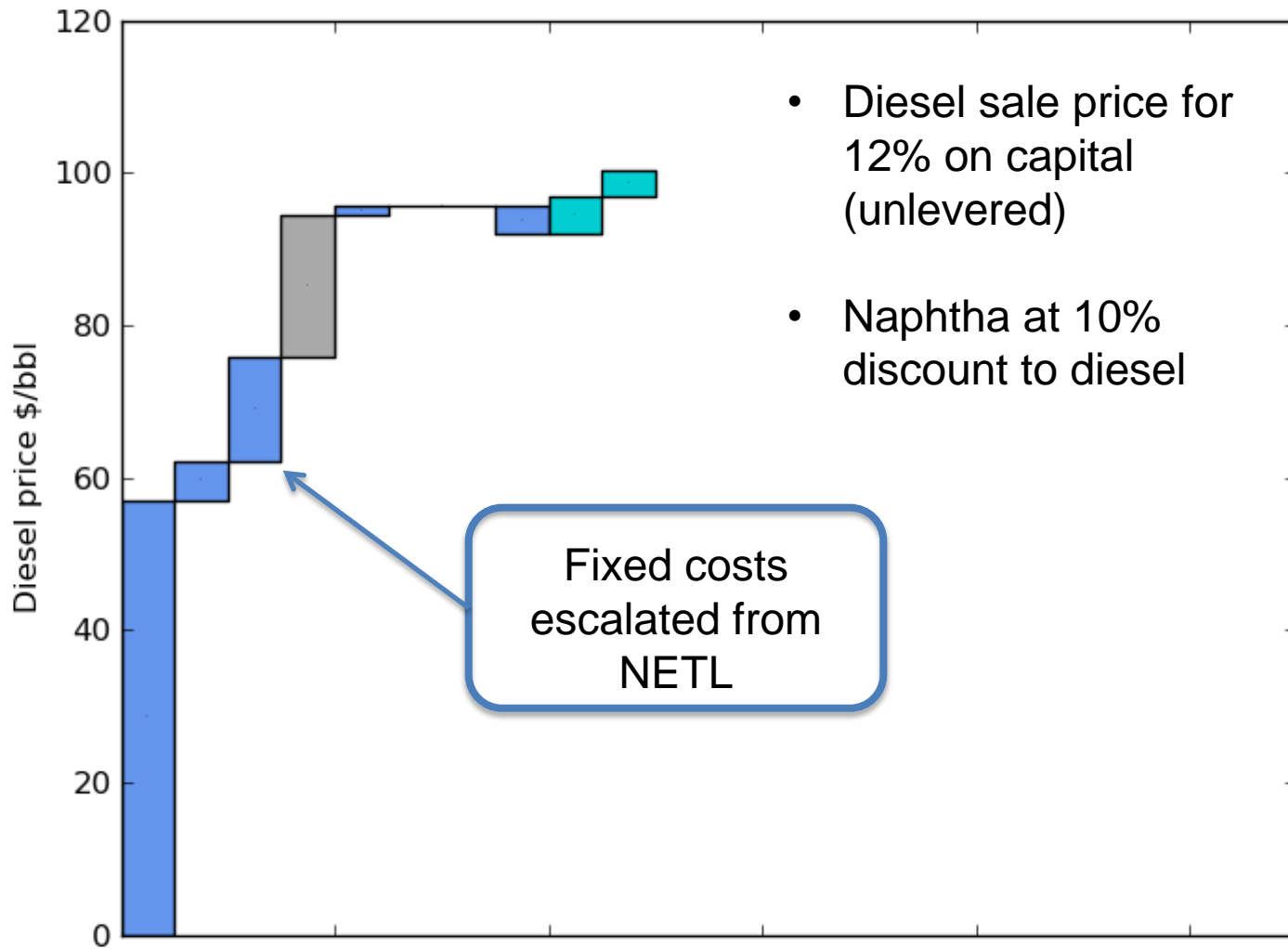
Capital costs

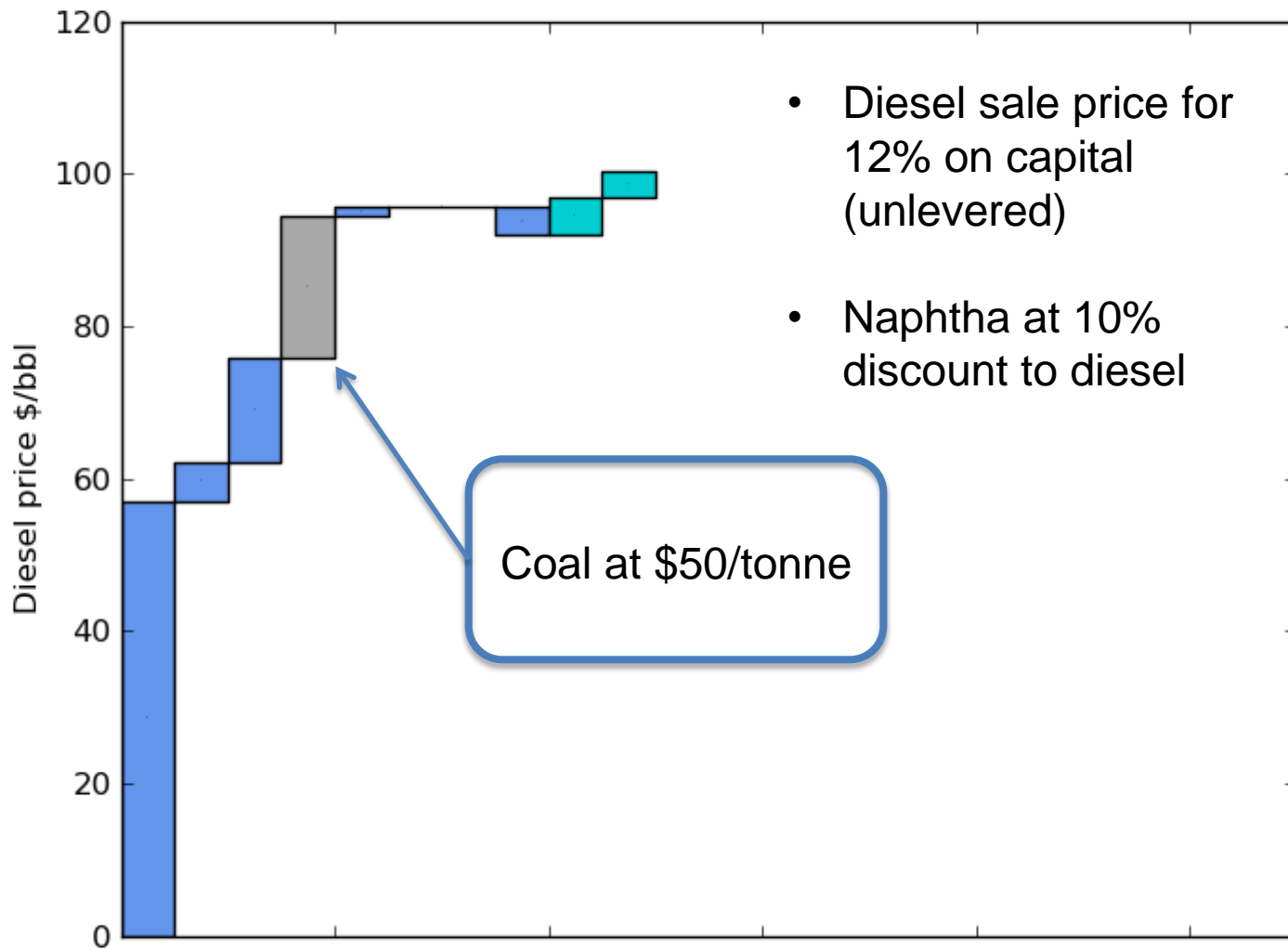
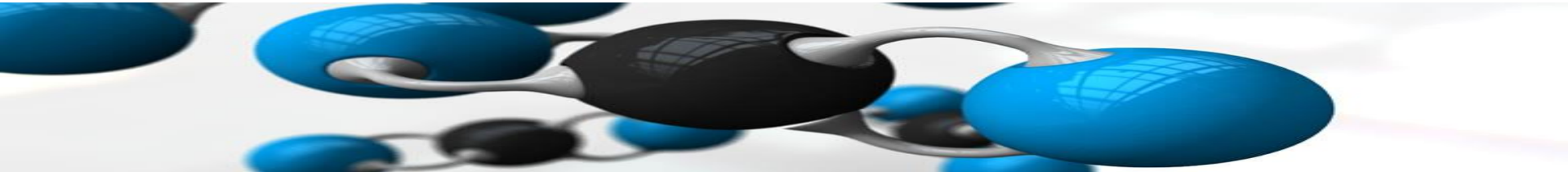
- From NETL study
- Escalated using CE process plant index
- Included allowance for site specific capital and for CO2 transport and storage infrastructure
- Nominal \$7,300M

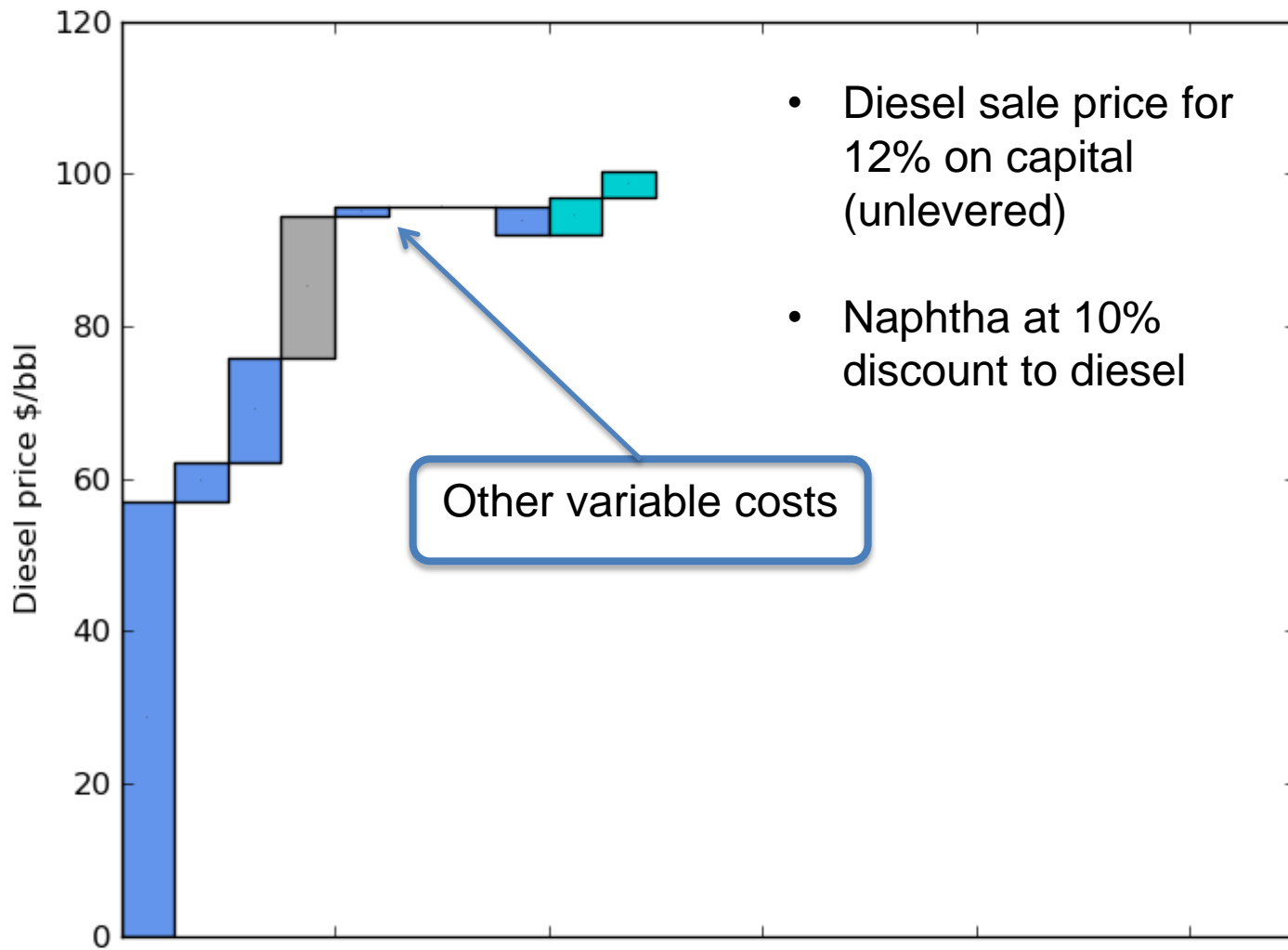
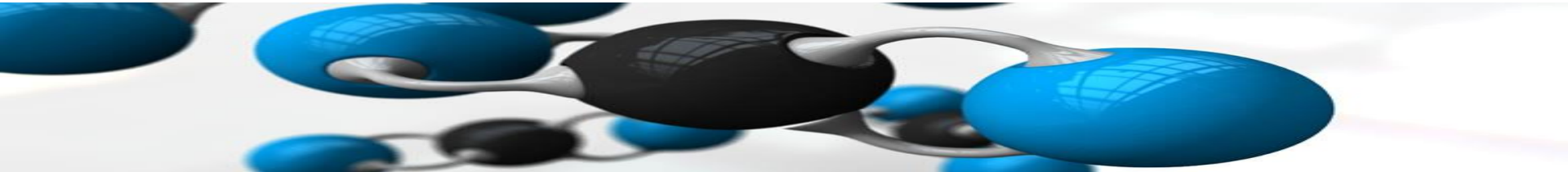
Item	\$k	%
EPC costs	2,807	100
Working capital	83	3
Process contingency	113	4
Project contingency	730	26
Startup	56	2
Owners costs	281	10
IDC	385	14
Financing fees	73	3
TOC for core plant (\$k 2006)	4,528	
TOC for core plant (\$k 2012)	5,737	
Site specific capital	500	
Transport and storage	500	
TOC for complete plant (2012)	6,737	

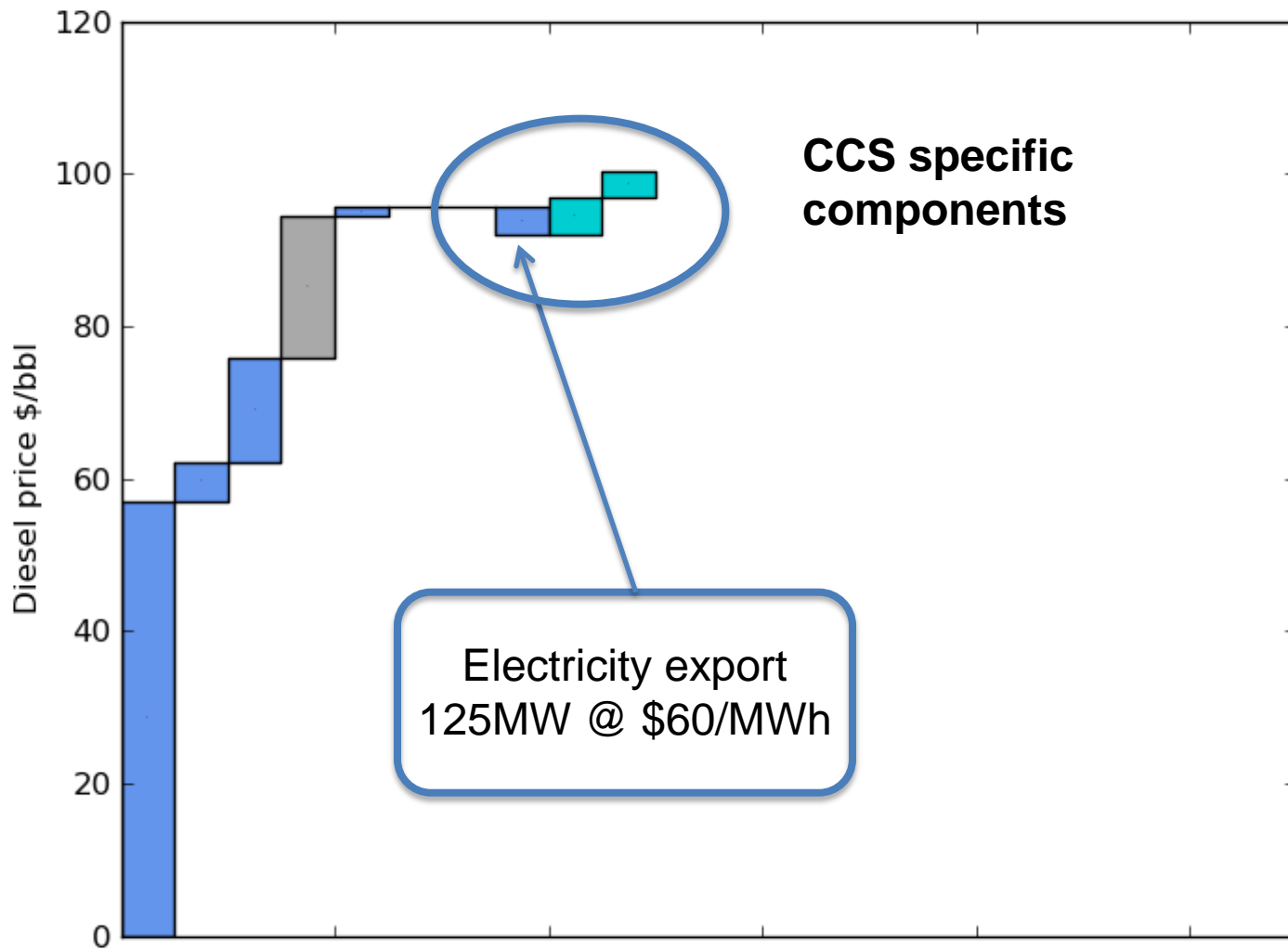
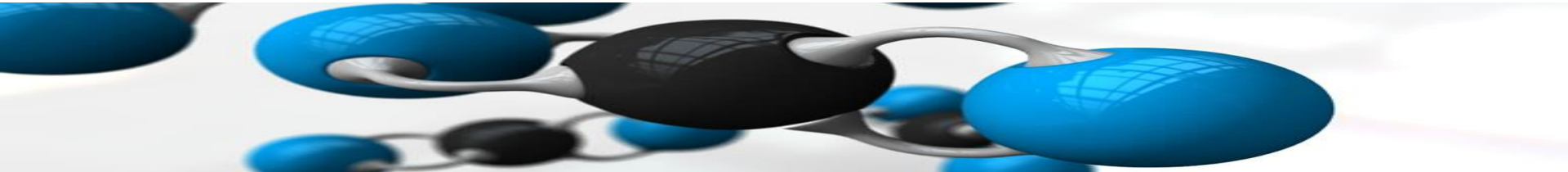


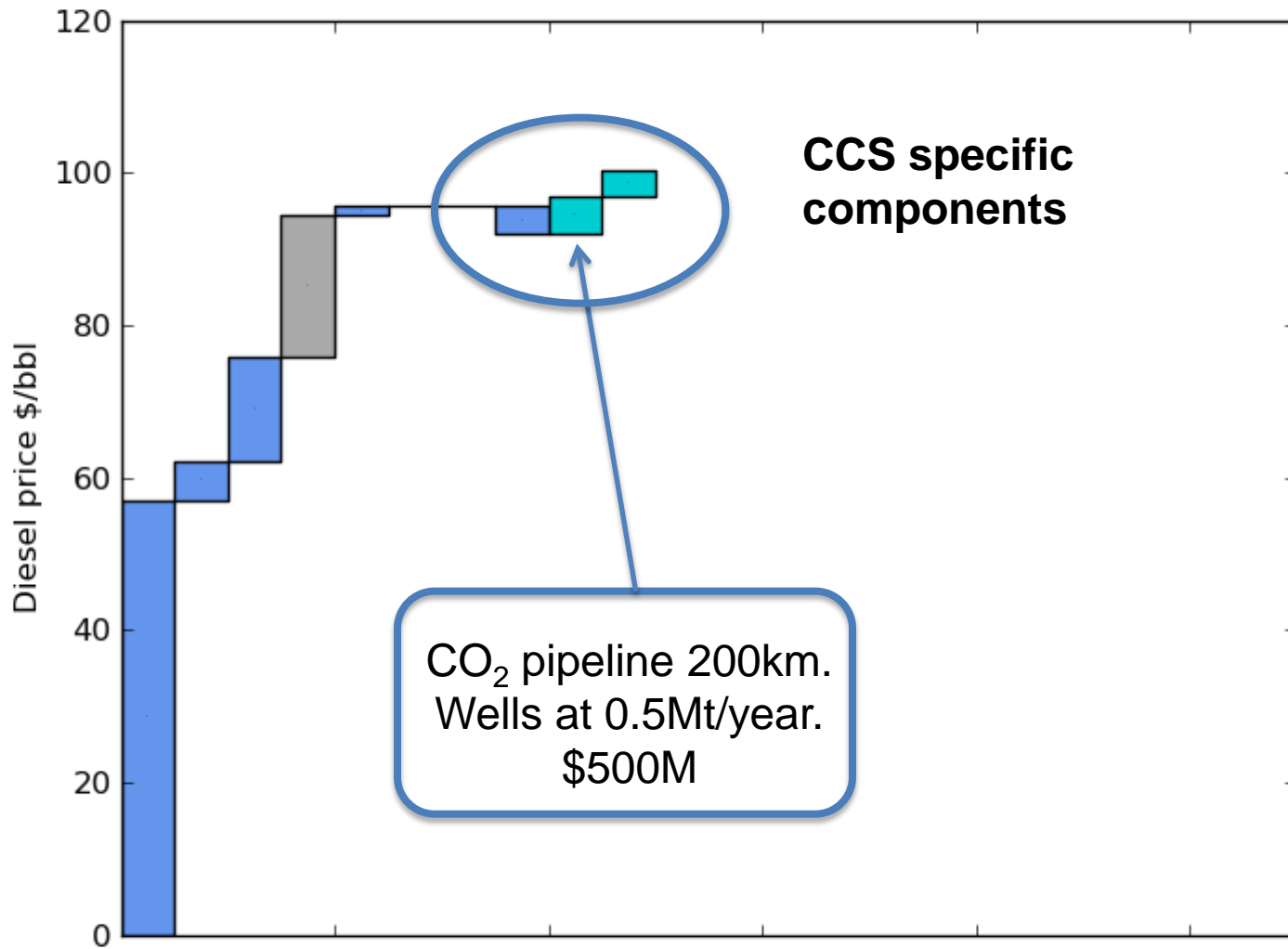


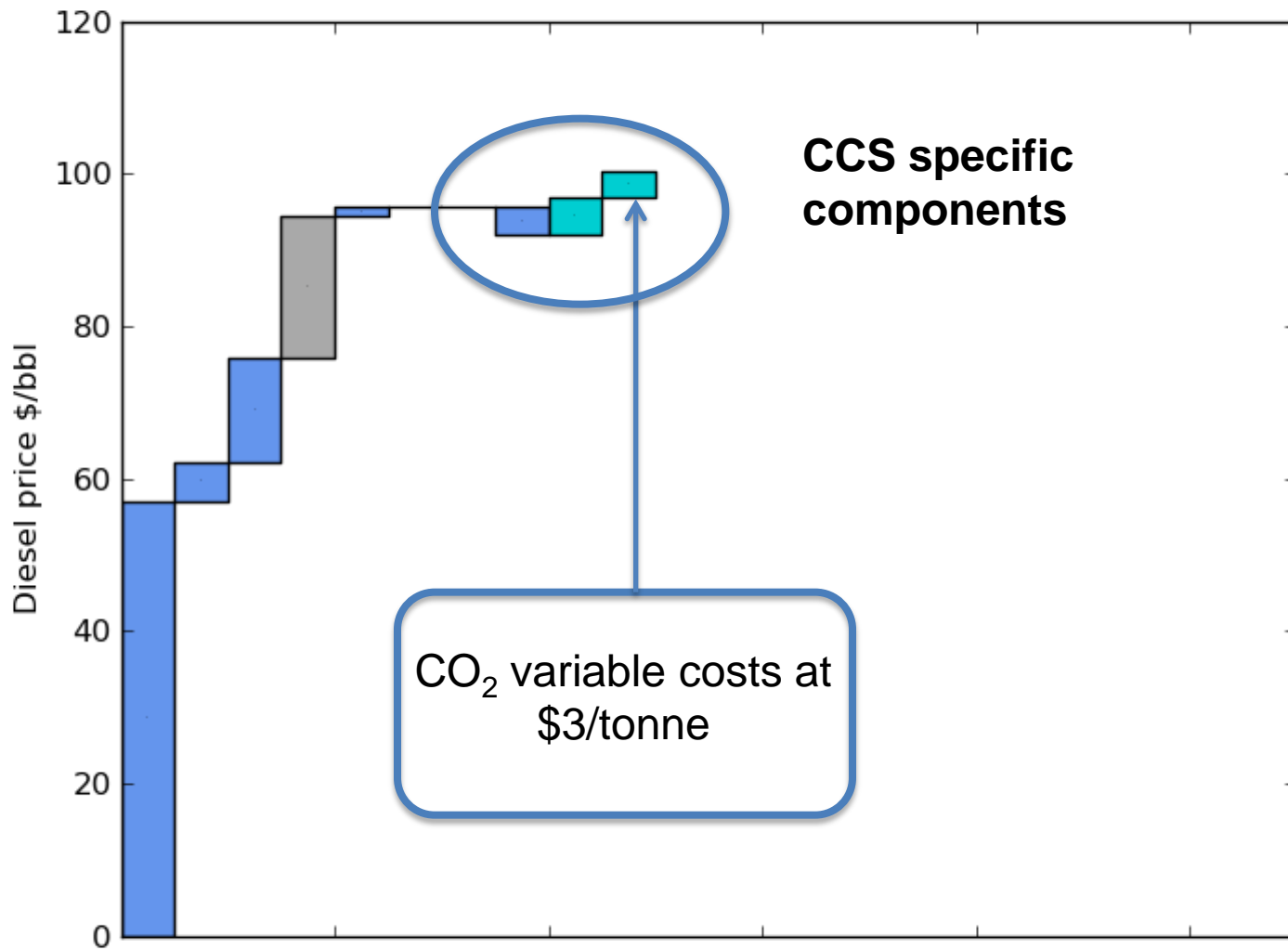
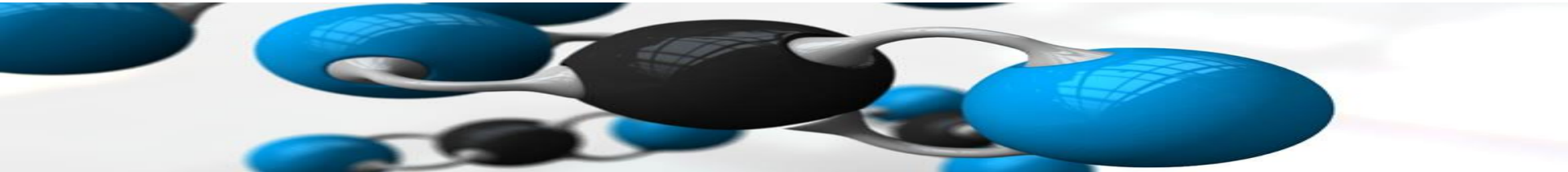




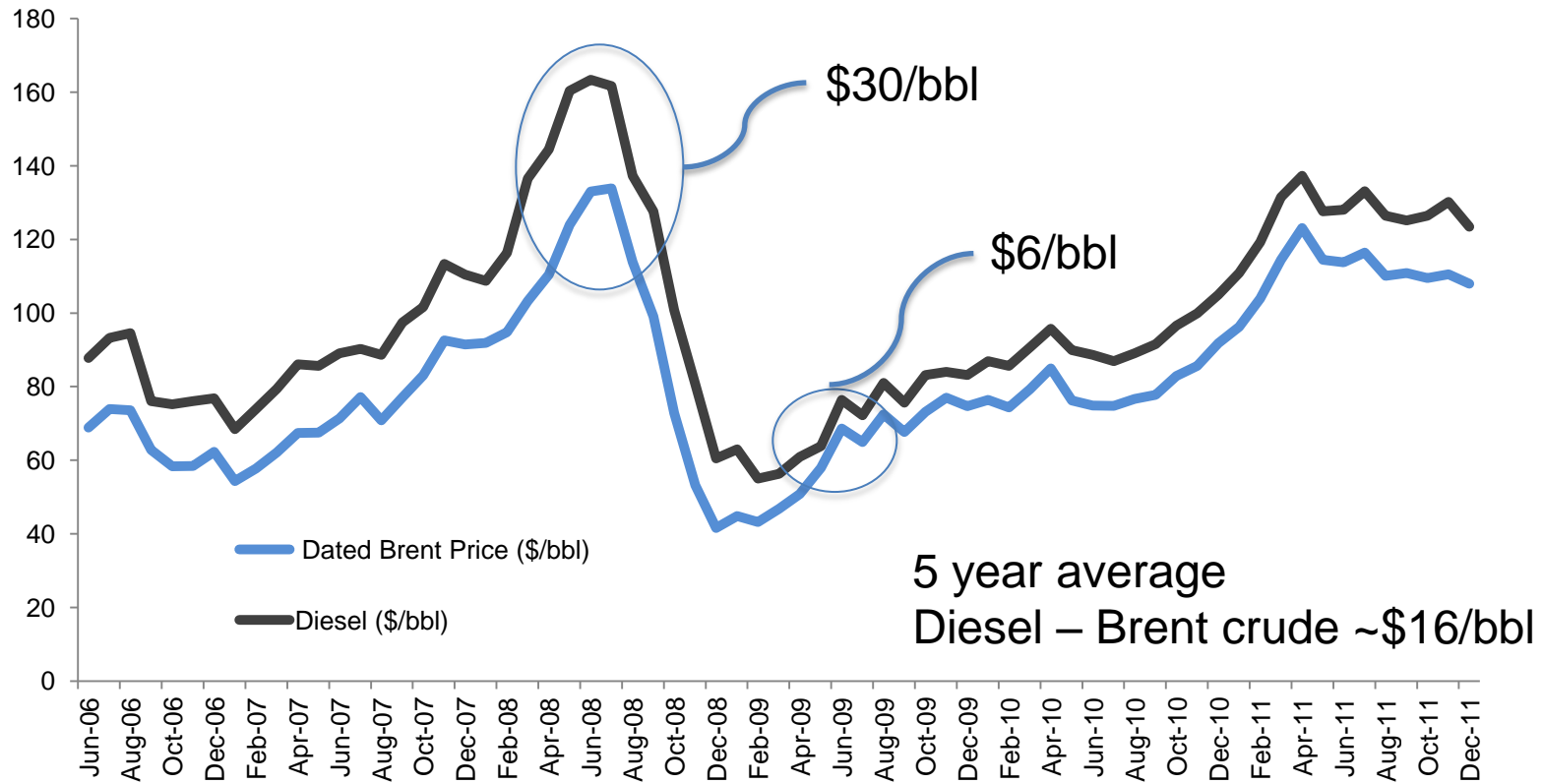


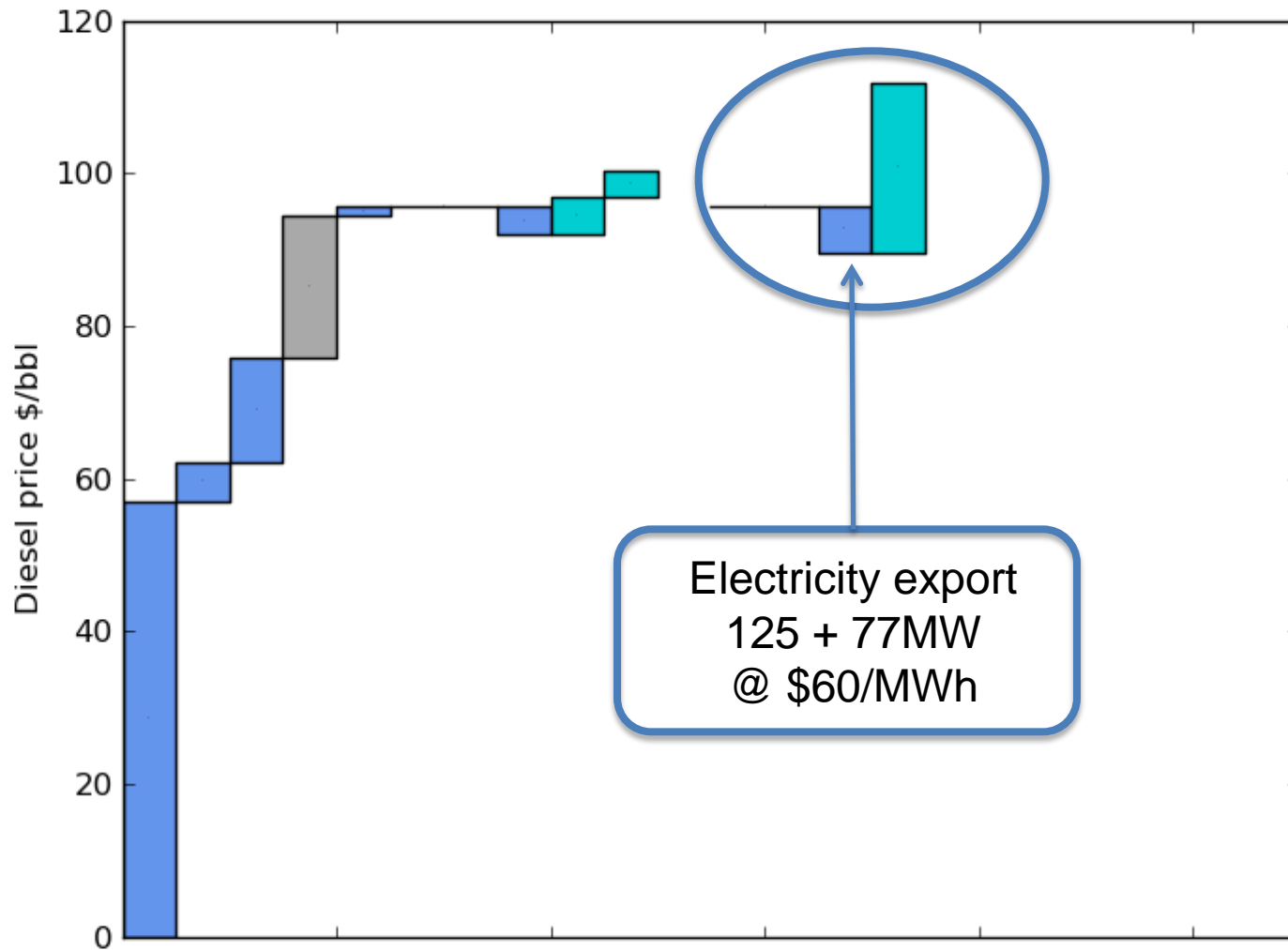




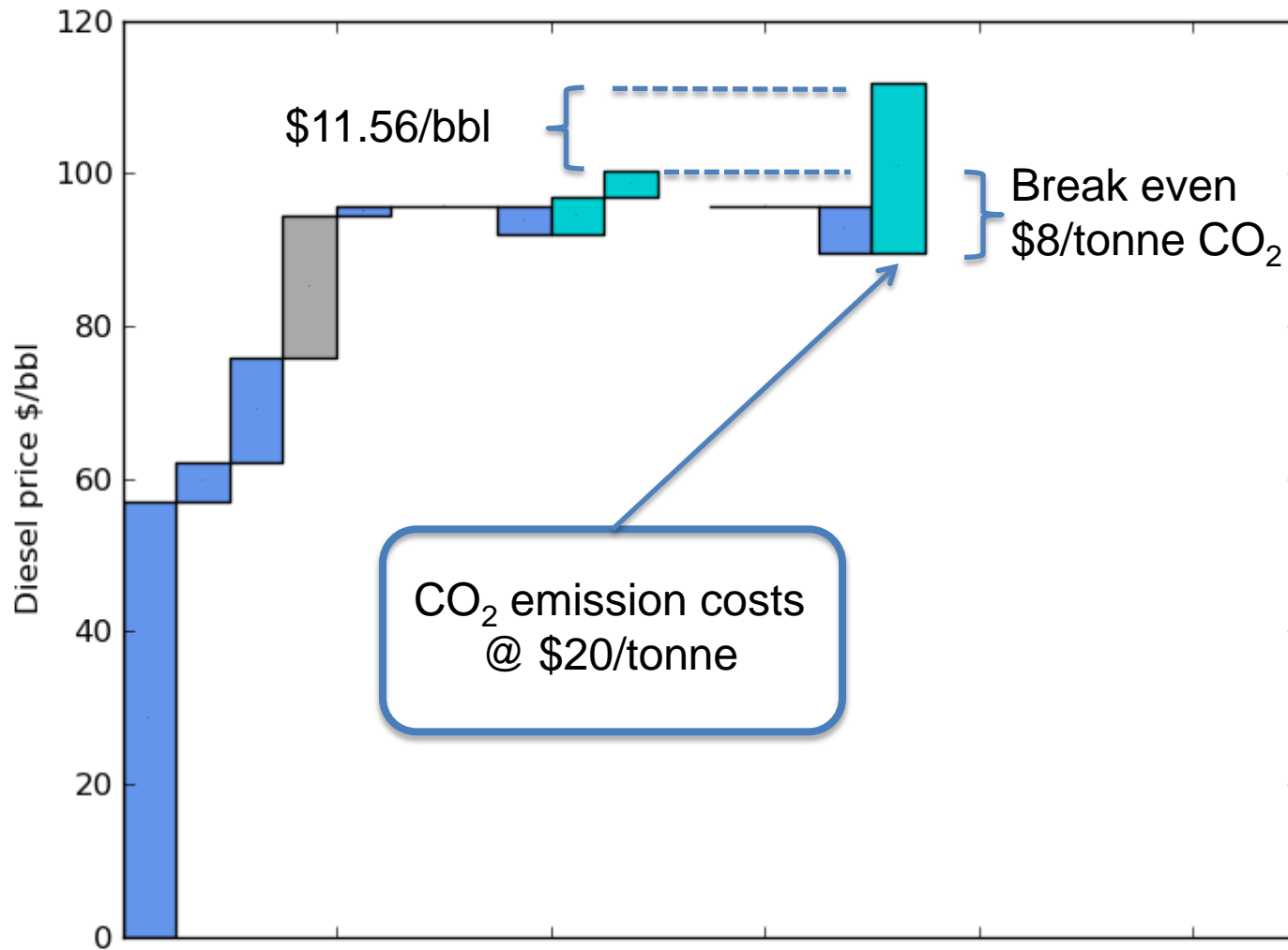


Historical crude/diesel price

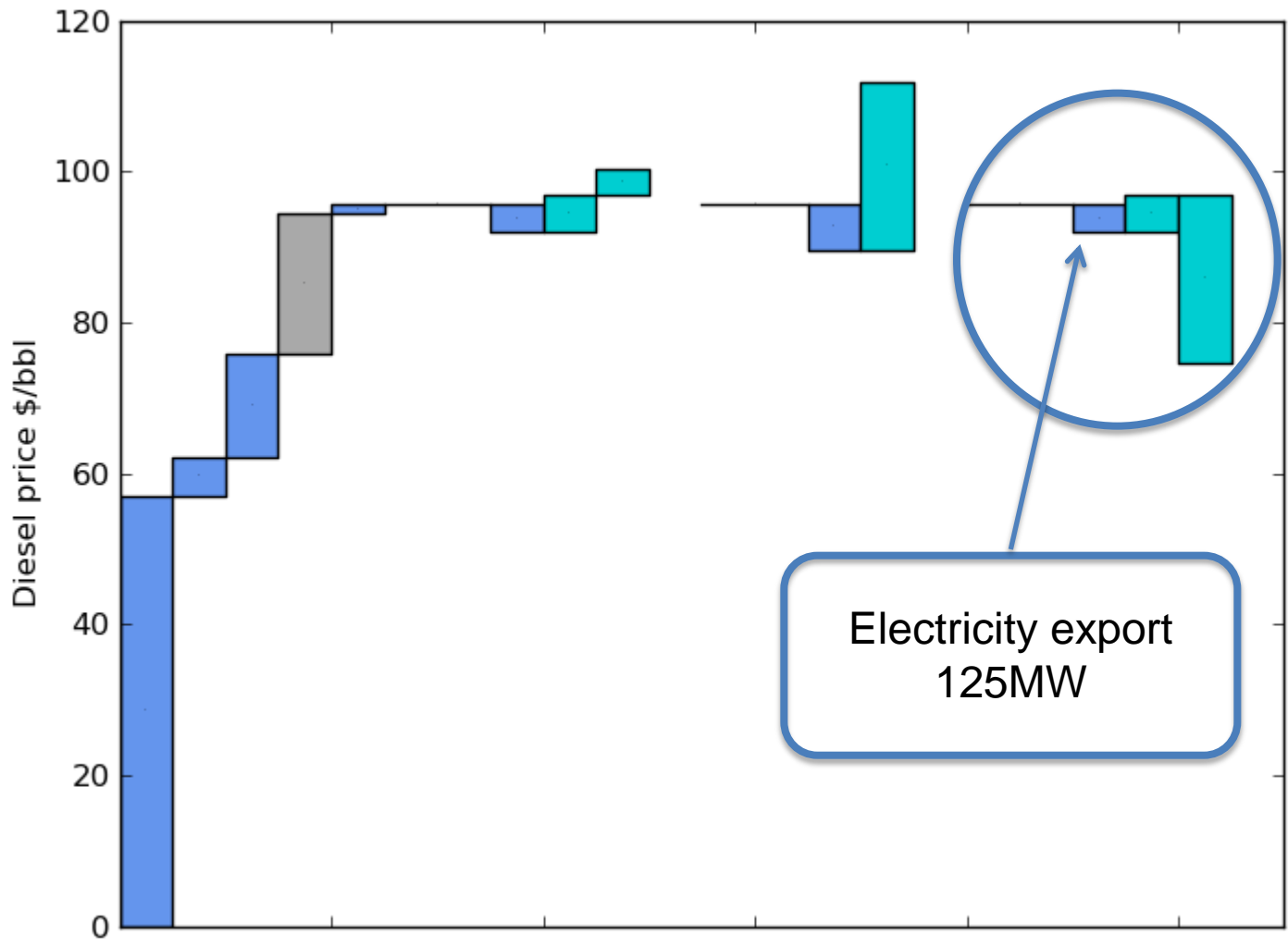




**Without CCS.
CO₂ vented**

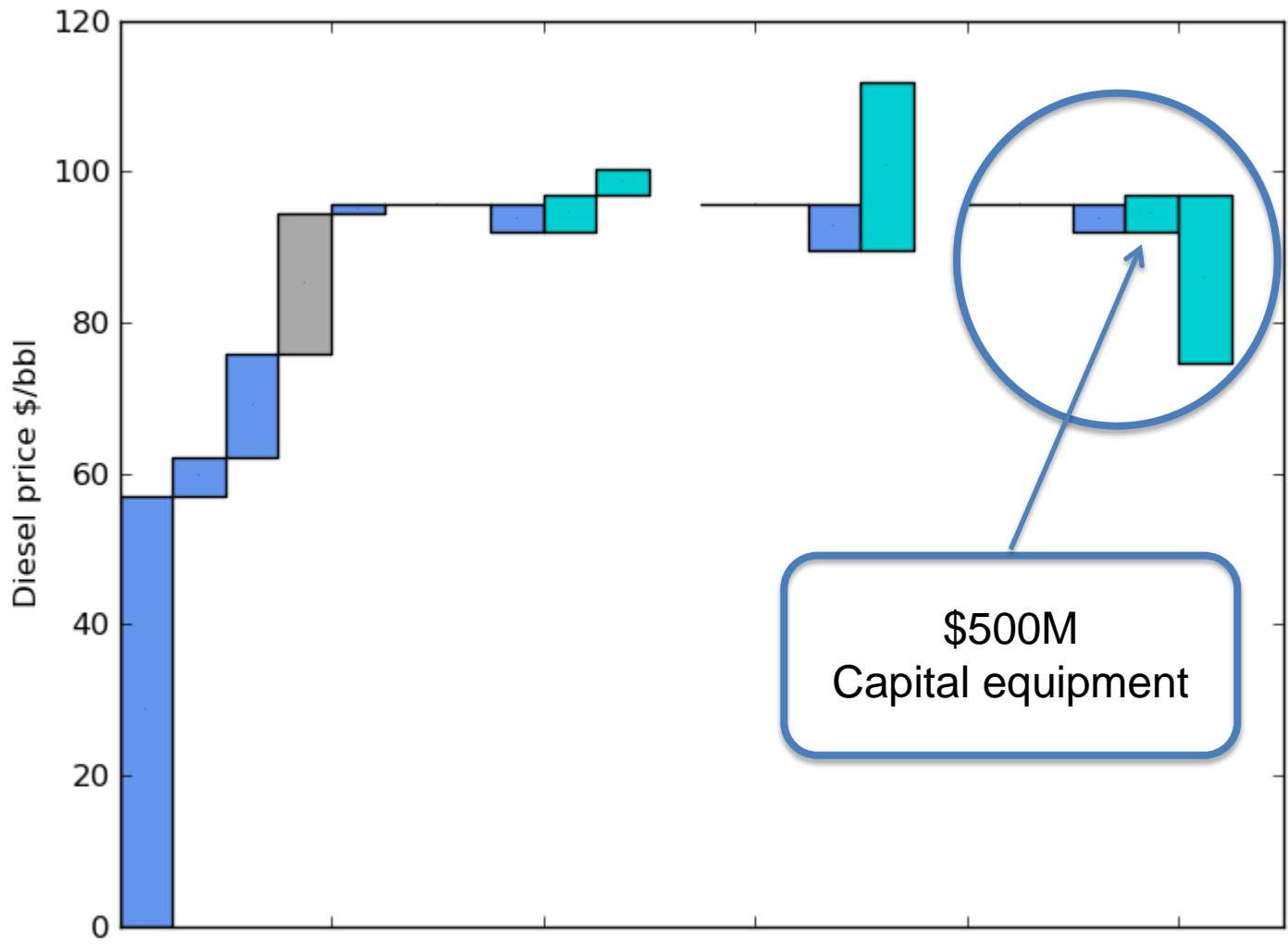


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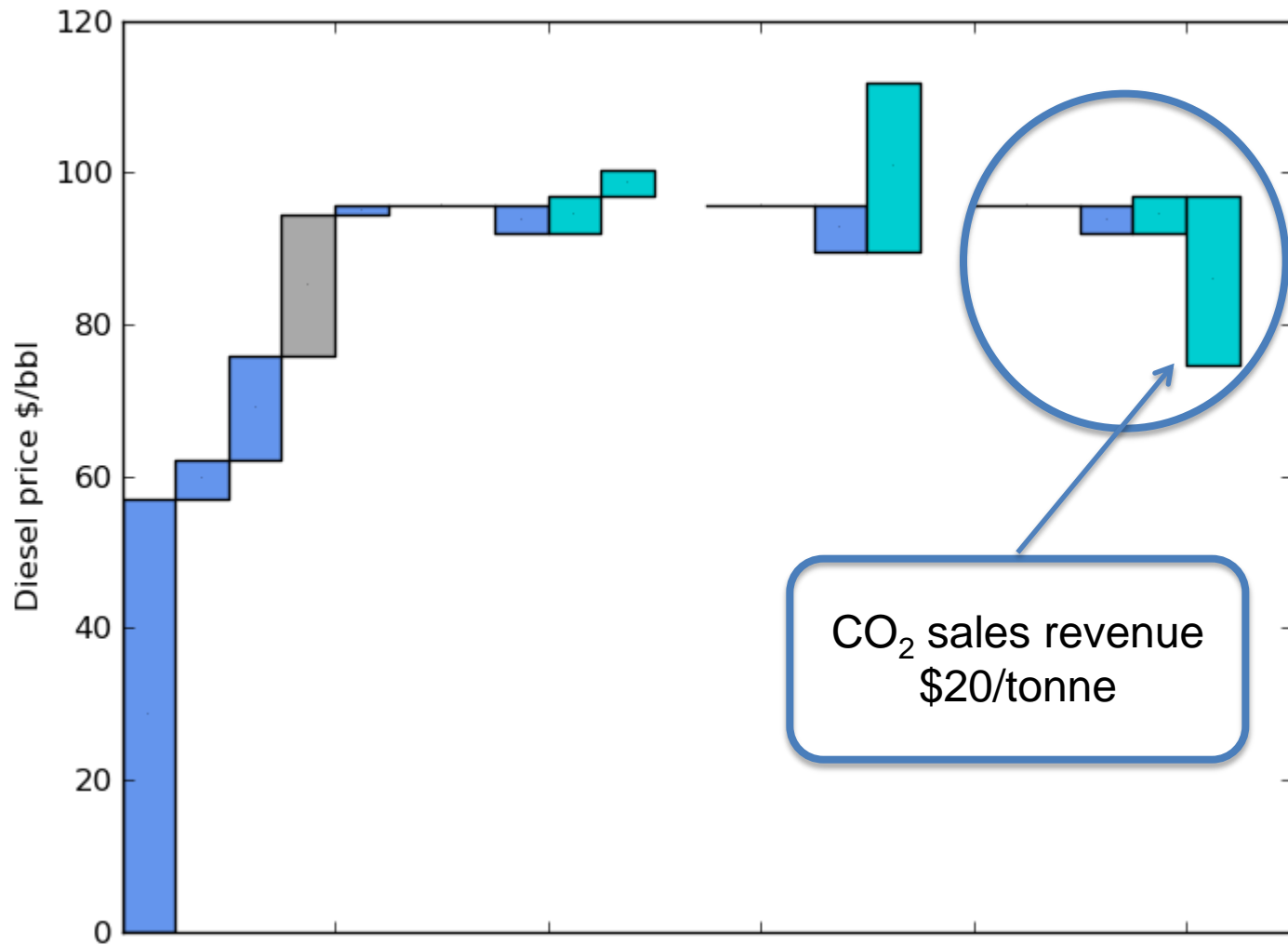
CO₂ to EOR

Electricity export
125MW



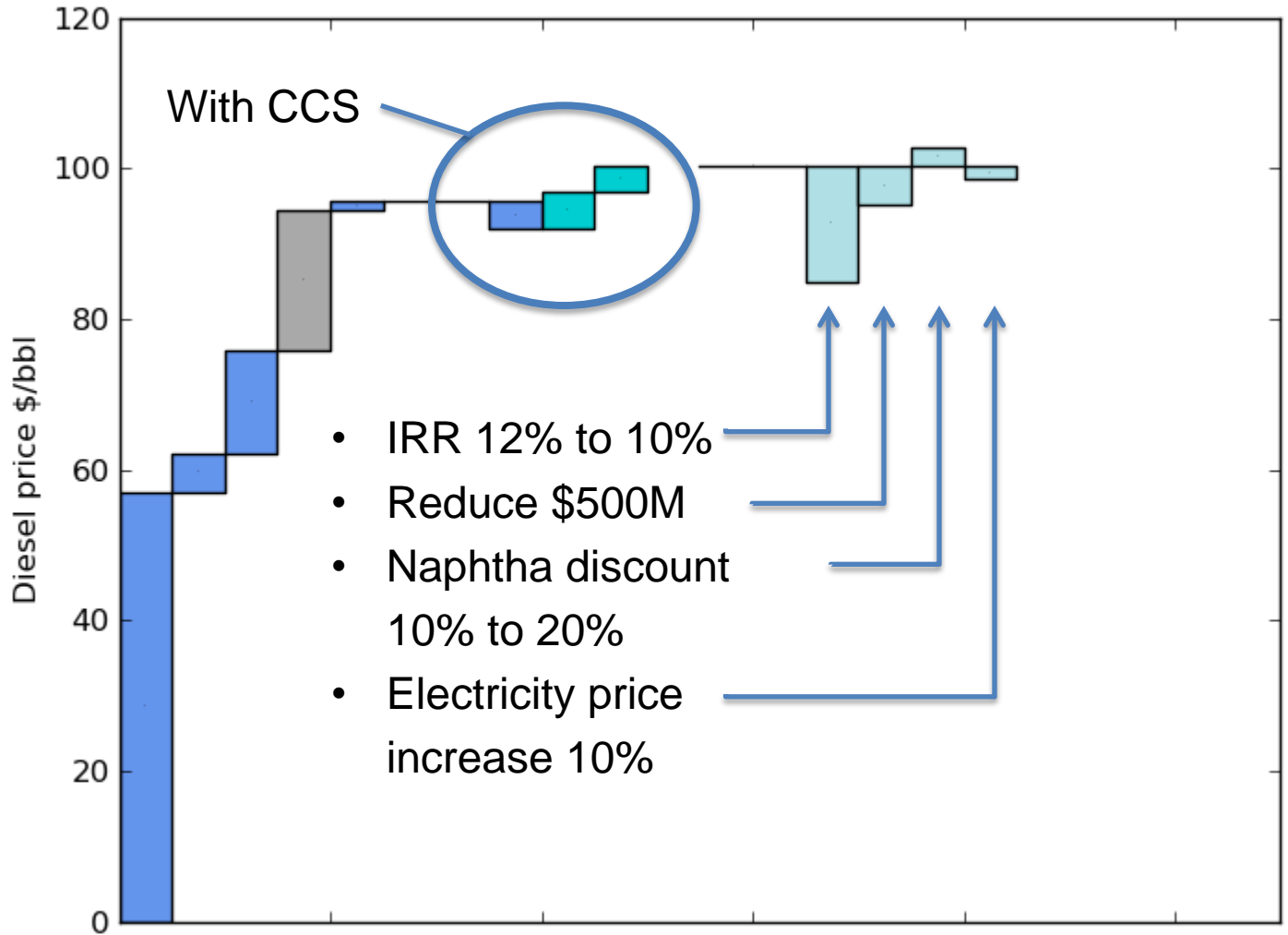
CO₂ to EOR

\$500M
Capital equipment



CO₂ to EOR

CO₂ sales revenue
\$20/tonne



Sensitivities



Observations

- CTL investments appear plausible at current oil prices.
- Investment decision is driven by confidence that oil price will remain high enough to cover enormous capital outlays
- Only a small CO₂ price (\$8/tonne) is required to make CCS break even compared to venting
 - Any policy to support CTL would need to address capital service in low oil price
 - Supporting CO₂ infrastructure would not materially influence investment economics but may change perception of risk.
- Advantaged locations:
 - Low construction cost
 - Access to “stranded” coal
 - Sales path for naphtha
 - EOR



Policy issues

- Security of supply and economics are the drivers. Not CO₂ reduction compared to mineral oil.
- Premise is that supporting CTL may stimulate CO₂ infrastructure and CCS development.
- Value of CO₂ infrastructure (in this case) is \$500M. How does this compare to covering downside crude price risk on \$7B?
 - Liquid fuel supply security may influence this balance
- CTL may happen spontaneously (or with small incentives) in advantaged locations.
 - Where are these advantaged locations and do they fit with CCS for power?
 - Can we engage the Oil and Gas industry in this effort?